



Slipstream pilot plant demonstration of an amine-based post-combustion capture technology for CO₂ capture from coal-fired power plant flue gas

DOE funding award DE-FE0007453

2012 NETL CO₂ Capture Technology Meeting

Krish R. Krishnamurthy, Linde LLC

July 9-12, 2012

Pittsburgh, PA

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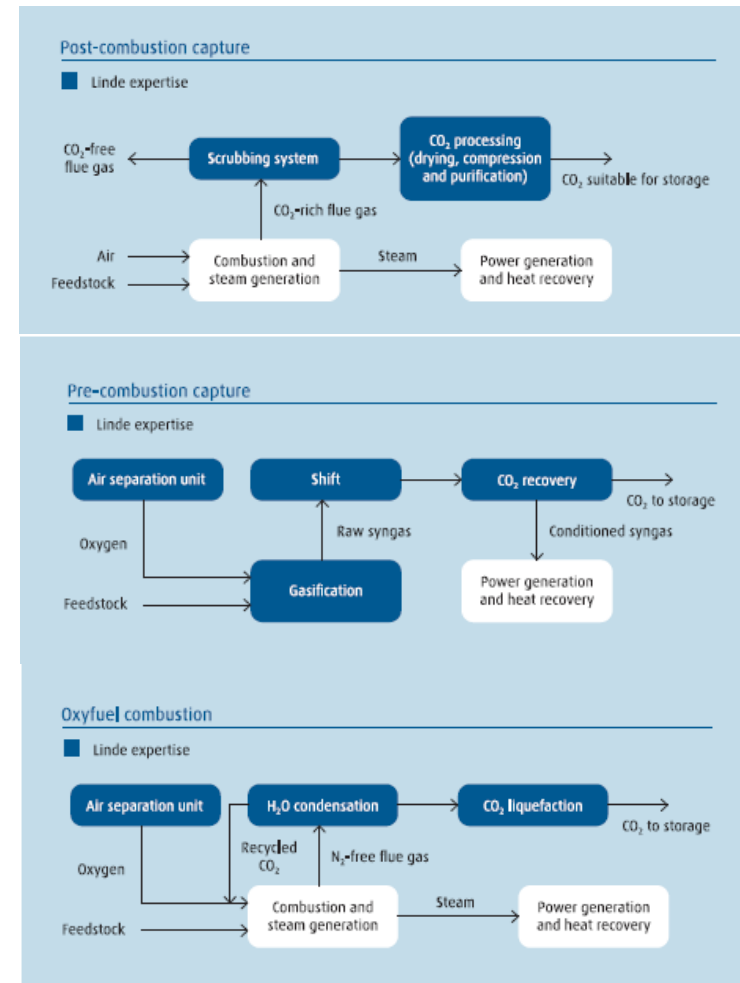


Linde

The Linde Group Overview and Carbon Capture Expertise

Founded	1879
Sales (2011)	\$18 billion
Employees	50,000
Countries	>100
US Linde Gas HQ	Murray Hill, NJ
US Linde Engineering Facilities	Blue Bell, PA; Tulsa, OK & Holly Springs, GA

Linde pursues technology development and solution offer in all three CC pathways



Linde Engineering Technology-focused

Air Separation Global #1	Hydrogen/Syn Gas Global #2
Olefins Global #2	Natural Gas Global #3



Linde Gas - Tonnage World-class operations

HyCO Tonnage Plants >70 plants	ASU Tonnage Plants >300 plants
CO₂ Plants >100 plants	ECOVAR Std Plants >1,000 plants

Project Participants



Partner/ Organization	Lead contact(s)	Key Role(s)
DOE-NETL	Andrew P. Jones, Project Manager	-Funding & Sponsorship
Linde LLC	Krish Krishnamurthy, PI Stevan Jovanovic, Technical Lead	-Prime contract -Overall program management -Operations and testing
BASF	Iven Clausen (BASF SE) Sean Rigby (BASF Corp)	-OASE® blue technology owner -Basic design -Solvent supply and analysis
EPRI	Richard Rhudy	-Techno-economics review -Independent validation of test analysis and results
Southern Co./NCCC	Frank Morton Michael England	-NCCC Host site (Wilsonville, AL) -Infrastructure and utilities for pilot plant build and operations
Linde Engineering, Dresden	Torsten Stoffregen Harald Kober	-Basic engineering -Support for commissioning -Operations and testing
SFPC (Linde Eng)	Lazar Kogan	-Detailed engineering -Procurement and installation

Project Objectives

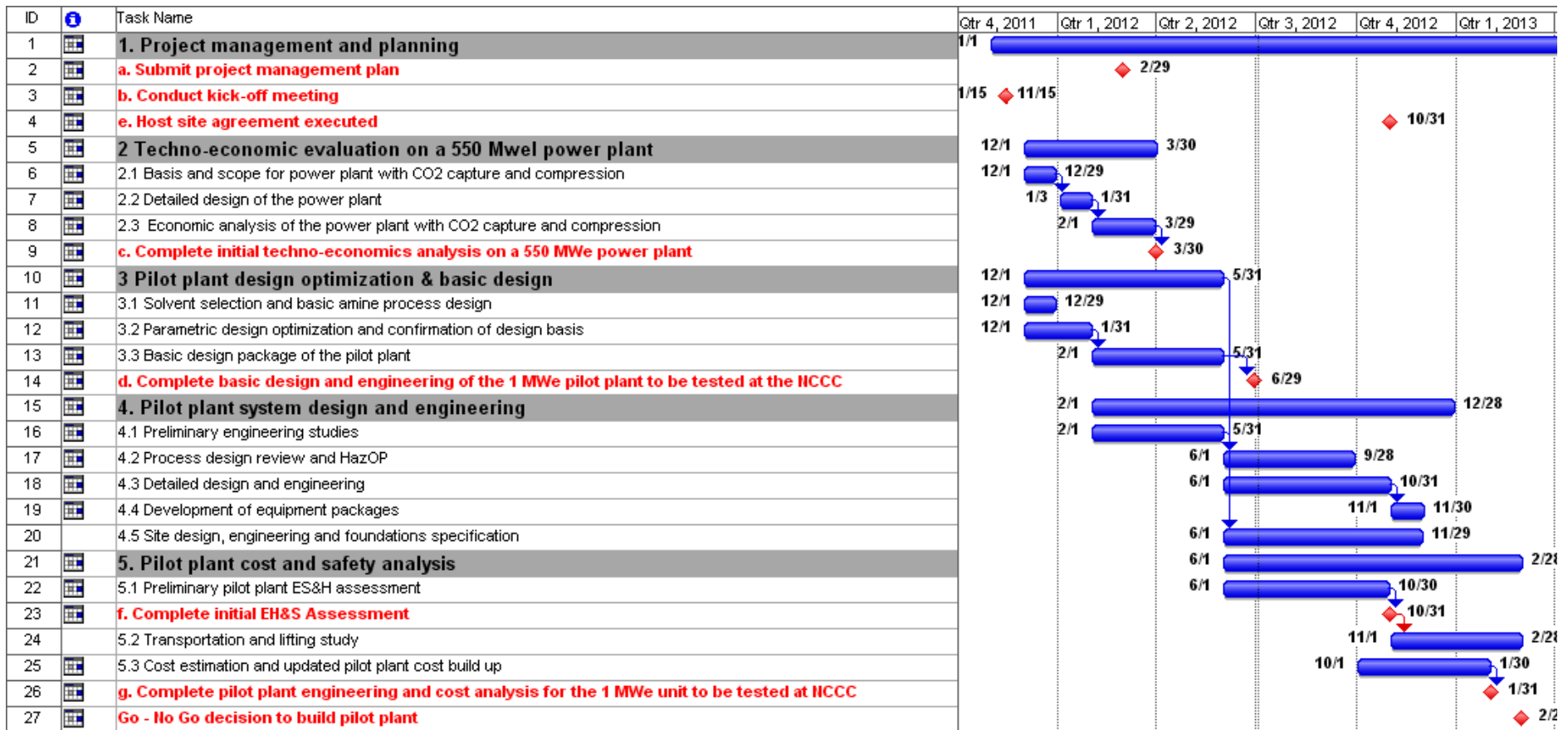
Overall Objective

- Demonstrate Linde-BASF post combustion capture technology by incorporating BASF's amine-based solvent process in a 1 MWel slipstream pilot plant and achieving at least 90% capture from a coal-derived flue gas while demonstrating significant progress toward achievement of DOE target of less than 35% increase in levelized cost of electricity (LCOE)

Specific Objectives

- Complete a techno-economic assessment of a 550 MWel power plant incorporating the Linde-BASF post-combustion CO₂ capture technology to illustrate the benefits
- Design, build and operate the 1MWel pilot plant at a coal-fired power plant host site providing the flue gas as a slipstream
- Implement parametric tests to demonstrate the achievement of target performance using data analysis
- Implement long duration tests to demonstrate solvent stability and obtain critical data for scale-up and commercial application

Project schedule and milestones: Budget Period 1



Budget Period 2: March 2013 to February 2014 (Pilot plant procurement, fabrication and installation)

Budget Period 3: March 2014 to November 2015 (Pilot plant operations, parametric and long-duration testing)

Project Budget: DOE funding and cost share

Source	Budget Period 1 Dec 2011 – Feb 2013	Budget Period 2 Mar 2013 – Feb 2014	Budget Period 3 Mar 2014 – Nov 2015	Total
DOE Funding	\$2,215,352	\$9,822,449	\$2,754,564	\$14,792,365
Cost Share	\$553,838	\$2,455,612	\$688,641	\$3,698,091
Total Project	\$2,769,190	\$12,278,061	\$3,443,205	\$18,490,456

Cost share commitments:

Linde: \$3,107,352

BASF: \$ 493,360

EPRI: \$ 97,379

Key Project Milestones (Budget Period 1)

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The Linde logo, featuring the word "Linde" in a white, cursive script font, set against a dark blue background with a light blue wavy graphic above it.

Budget Period 1 (Dec. 1, 2011 – Feb. 28, 2013)

- Submit project management plan (03/09/2012) ✓
- Conduct kick-off meeting with DOE-NETL (11/15/2011) ✓
- Complete initial techno-economic analysis on a 550 MWe₁ power plant (05/04/2012) ✓
- Complete basic design and engineering of a 1 MWe pilot plant to be tested at NCCC (06/20/2012) ✓
- Execute host site agreement (10/31/2012)
- Complete initial EH&S assessment (10/31/2012)
- Complete detailed pilot plant engineering and cost analysis for the 1 MWe pilot plant to be tested at NCCC (01/31/2013)

Key Project Milestones (Budget Periods 2 and 3)

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Budget Period 2 (Mar. 1, 2013 – Feb. 28, 2014)

- Complete purchase orders and fabrication contracts for the 1 MWe pilot plant (03/29/2013)
- Complete shop fabrication of equipment and modules and associated engineering checks (07/31/2013)
- Complete site preparation and foundation installations at NCCC to receive pilot plant (08/15/2013)
- Complete installation of the 1 MWe pilot plant at NCCC (11/30/2013)
- Mechanical completion of 1 MWe pilot plant at NCCC (02/28/2014)

Budget Period 3 (Mar. 1, 2014 – Nov. 30, 2015)

- Complete pilot plant start up and demonstrate plant operation at steady state (05/31/2014)
- Develop pilot-scale parametric test plan (06/30/2014)
- Complete 1 MWe pilot-scale parametric tests (11/30/2014)
- Develop pilot-scale long duration test plan (12/31/2014)
- Complete 1 MWe pilot-scale long duration tests (08/31/2015)
- Complete updated techno-economic analysis (10/31/2015)
- Complete updated EH&S assessment (11/30/2015)

Linde-BASF experience in large scale carbon capture

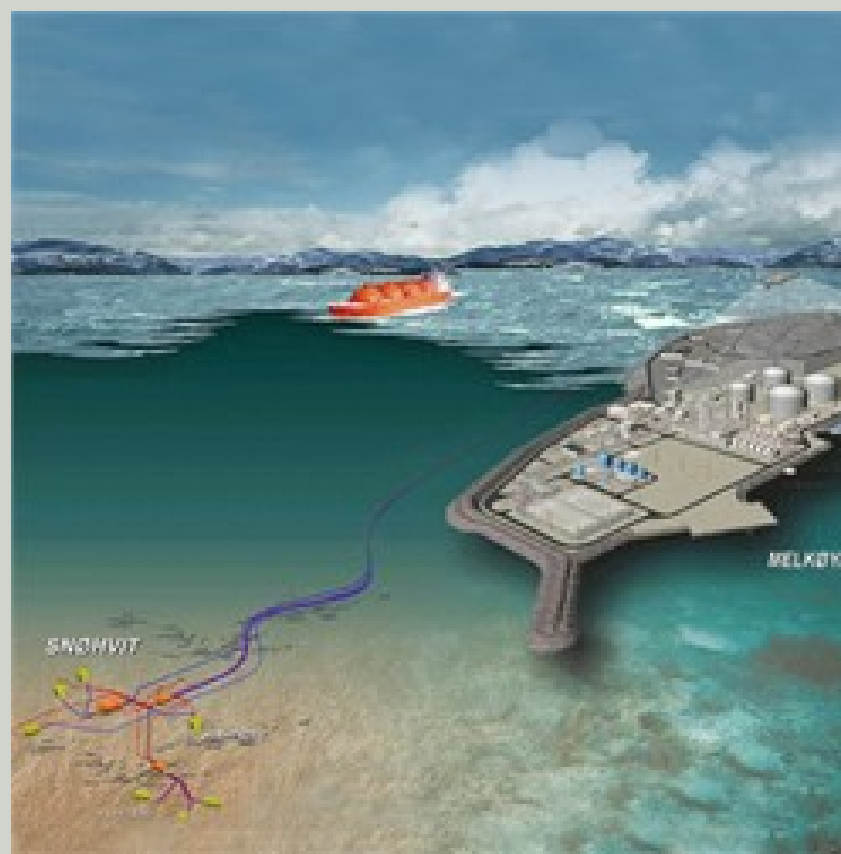
CO₂ capture in natural gas processing: Re-injection Project - Hammerfest



World's first industrial project to deliver CO₂ separated onshore from the well-stream back offshore for re-injection into a reservoir

- Partnership with StatoilHydro Petroleum
- Melkoya island near the town of Hammerfest, Norway
- CO₂ sequestration and re-injection integral part of the Hammerfest LNG project. **Linde performed design, EPC and commissioning**
- One dedicated well for CO₂ storage in a sandstone formation sealed by shale cap.
- Re-injection started in April 2008
- **BASF's OASE[®] purple process used in CO₂ capture**

700,000 tpa CO₂ capture and re-injection (part of world scale LNG project, Snøhvit, Norway)



Post combustion CO₂ capture: Challenges compared to CO₂ removal in NG/LNG plants

	NG/LNG	Flue gas
Pressure	50 – 100 bars	1 bara
CO ₂ partial pressure	1 – 40 bars	30 – 150 mbars
Flowrate	up to 60 mio scf/hr	up to 120 mio scf/hr
Gas composition	CH ₄ , C ₂ H ₆ , ..., CO ₂ , H ₂ S, COS, C _x H _y S, H ₂ O	N ₂ , O ₂ , H ₂ O, CO ₂ , (SO _x) NO _x
Treated gas specification	50 ppm – 2 % CO ₂ S < 4 – 10 ppm	CO ₂ removal rate (90 %) low amine emissions
Energy efficiency	not a key issue	of highest priority η ↘ 7-10% points



- large volume flows @ low pressure
- solvent stability
- emissions of solvent
- overall power plant efficiency losses

BASF OASE[®] blue Technology Development Designed for PCC Applications

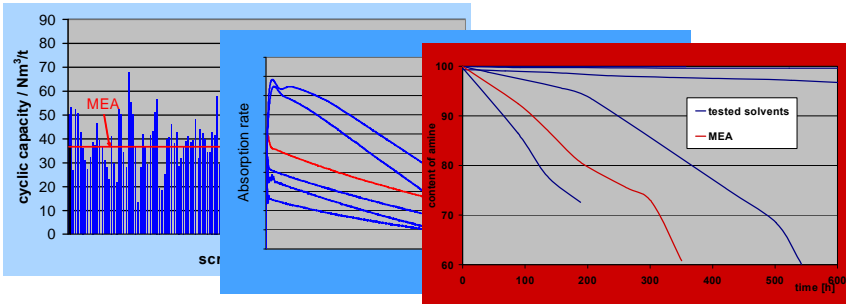
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Equilibrium **Kinetics** **Stability**

Fundamental Lab Scale R&D:
Advanced Solvents Screening,
Development, Optimization



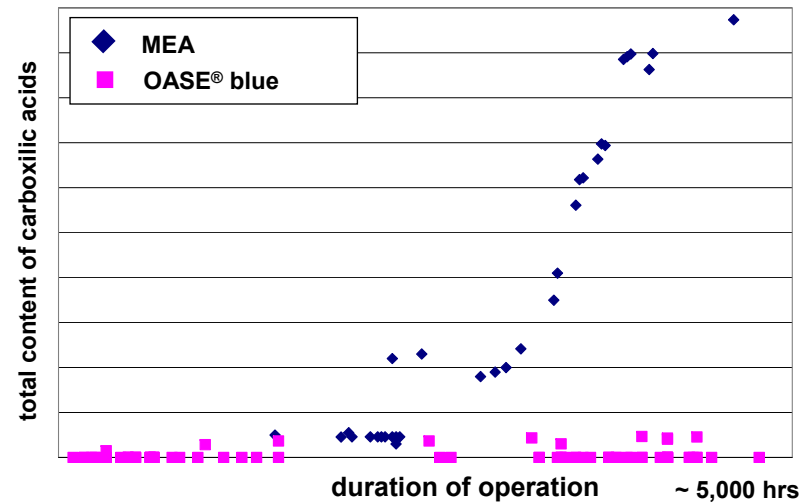
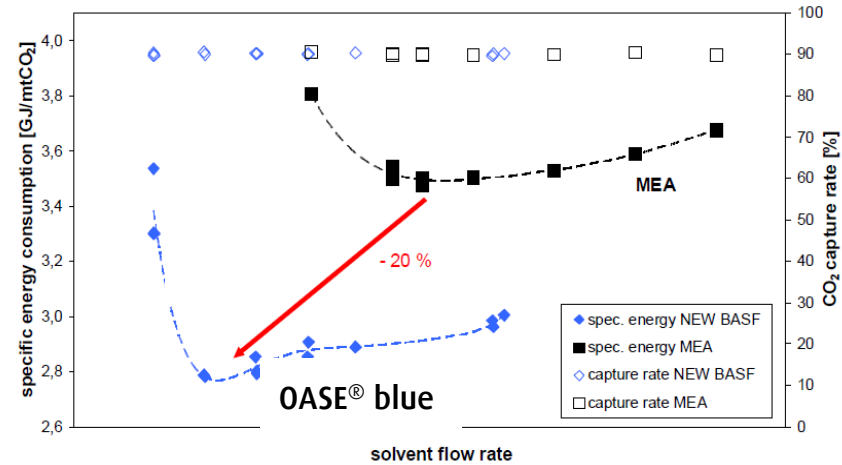
BASF Miniplant,
Ludwigshafen, Germany:
Solvent Performance
Verification



0.45 MWe PCC Pilot,
Niederaussem, Germany:
Preliminary Process
Optimization



Niederaussem* pilot plant key results



>90% carbon capture rate achieved

>20% improvement in specific energy compared to MEA

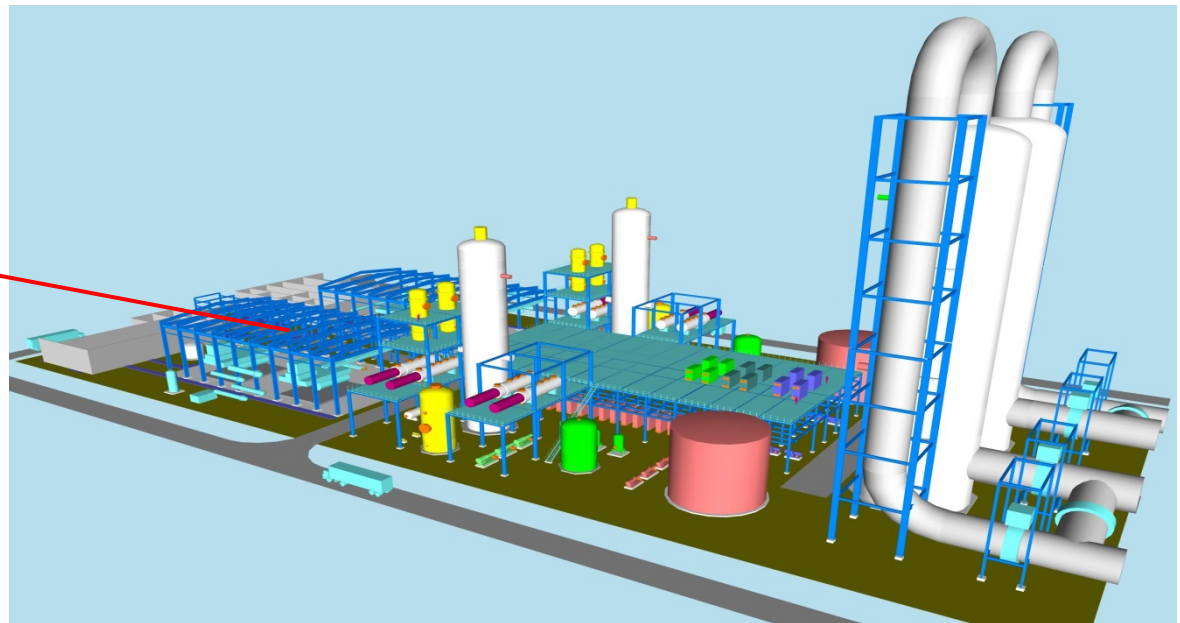
New BASF solvent is very stable compared to MEA

Acknowledgement: * Pilot project partner RWE

Solutions for Large Scale PCC Plant (1100 Mw_{el} Power) Design challenges

- Optimizing CAPEX by reduced number of trains to handle 18,000 tpd CO₂
- 2 process trains selected
 - reduced plot space

Compressor section
two lines per train
→ flexible turn down operation



Lower number of trains results in bigger size of components, e.g.

- Absorption column: diameter ca.18 m, height ca. 75 m → on site fabrication required
- Pipes ducts and valves: diameters up to 7 meters
- Plot : ca. 100 m x 260 m

Concepts for a Large Scale PCC Plant

Key elements of plant costs

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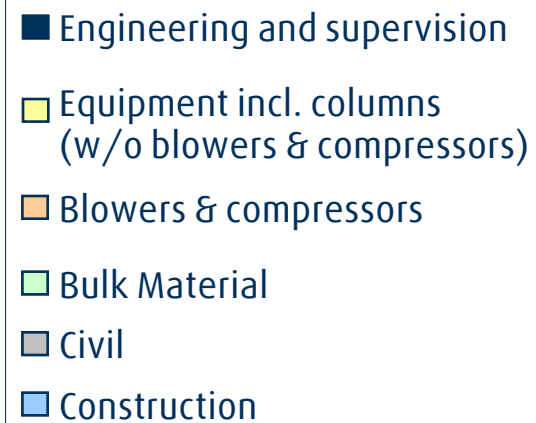
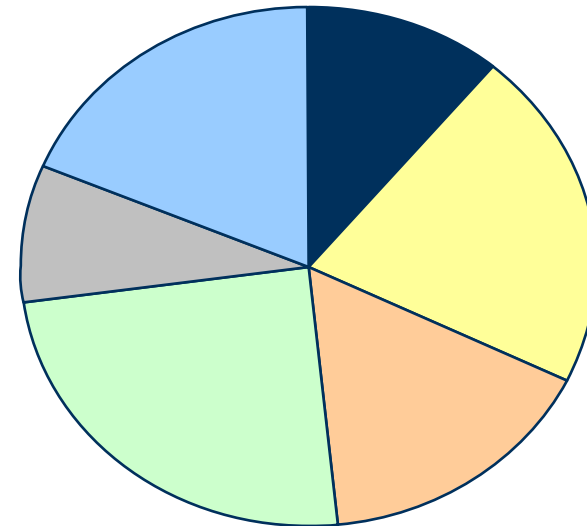
Main challenges

- Large equipment size requires new concepts
- Required plot area is very significant
- Alternative materials need to be assessed
- New equipment arrangements needed
- Field fabrication
- Large pipe and duct

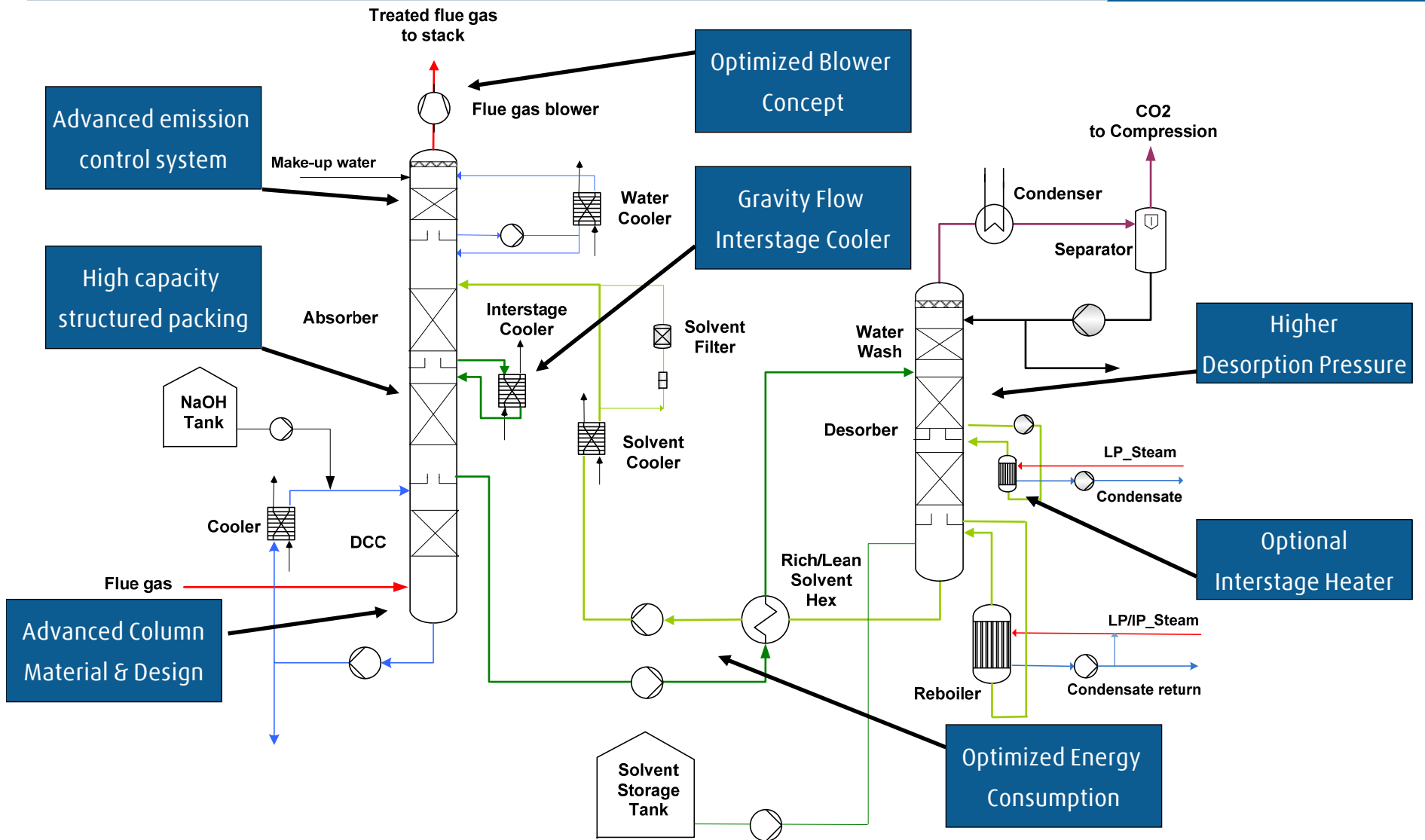
Linde studies to address challenges

- Scaling to a very large single train
- Optimize equipment arrangement (flue gas blower, pre-cooler, absorption columns sump etc)
- Develop new column construction materials
- Optimize machinery options

Total plant cost distribution



Linde-BASF advanced PCC plant design*



*Patent Applications 2010-2012

Source: Project DE-FE0007453 Techno-economic analysis of 550 MWe PC power plant with CO₂ capture, May 2012.

Project progress and accomplishments

Task#	Task Description	Key Objectives	Accomplishments
1	Program Management	Complete project management plan and implement to agreed cost and schedule.	<ul style="list-style-type: none"> - Project kick-off meeting held - Updated project management plan completed
2	Techno-economic evaluation	Complete techno-economic analysis on a 550 MWe coal-fired power plant incorporating Linde-BASF PCC technology.	<ul style="list-style-type: none"> - Techno-economic assessment completed and presented to DOE-NETL
3	Pilot plant optimization and basic design	Define pilot plant design basis and the key features incorporated. Complete basic design and engineering.	<ul style="list-style-type: none"> - Design basis document completed and pilot plant features selected. - Basic design and engineering completed.
4	Pilot plant system design and engineering	Complete detailed design and engineering of the pilot plant (ready to build).	<ul style="list-style-type: none"> - Preliminary 3-D model developed - Detailed engineering in progress (30% model)
5	Pilot plant cost and safety analysis	Complete preliminary environment, health and safety assessment for the pilot plant	<ul style="list-style-type: none"> - Preliminary NEPA document completed. - Hazop review completed and design updates incorporated.

Basis for techno-economic assessment for 550 MW_e power plant with 90% CO₂ capture

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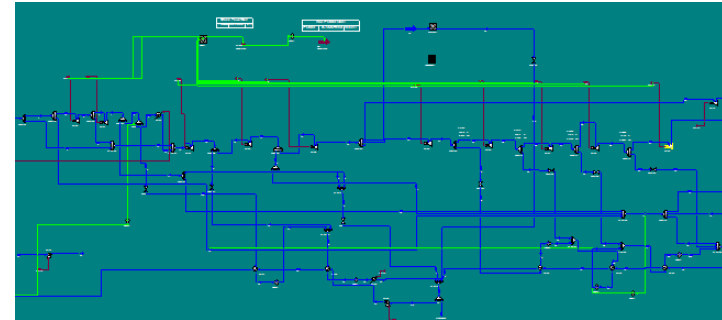
Specifications and Design Basis

identical to DOE/NETL Report 2007/1281

as per DE-FOA-0000403 requirements

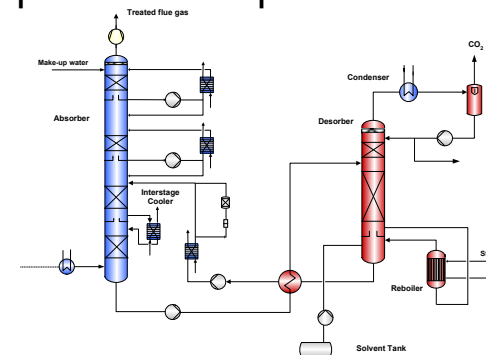
- Bituminous Illinois #6 Coal Characteristics
- Site Characteristics and Ambient Conditions
- Pulverized Coal Boiler Design
- Subcritical Steam Turbine Design
- Steam Cycle Conditions
- Environmental Controls and Performance
- Balance of Plant
- Economic Assumptions and Methodology

Computational Platform



UniSim Design Suite R390, integrated with

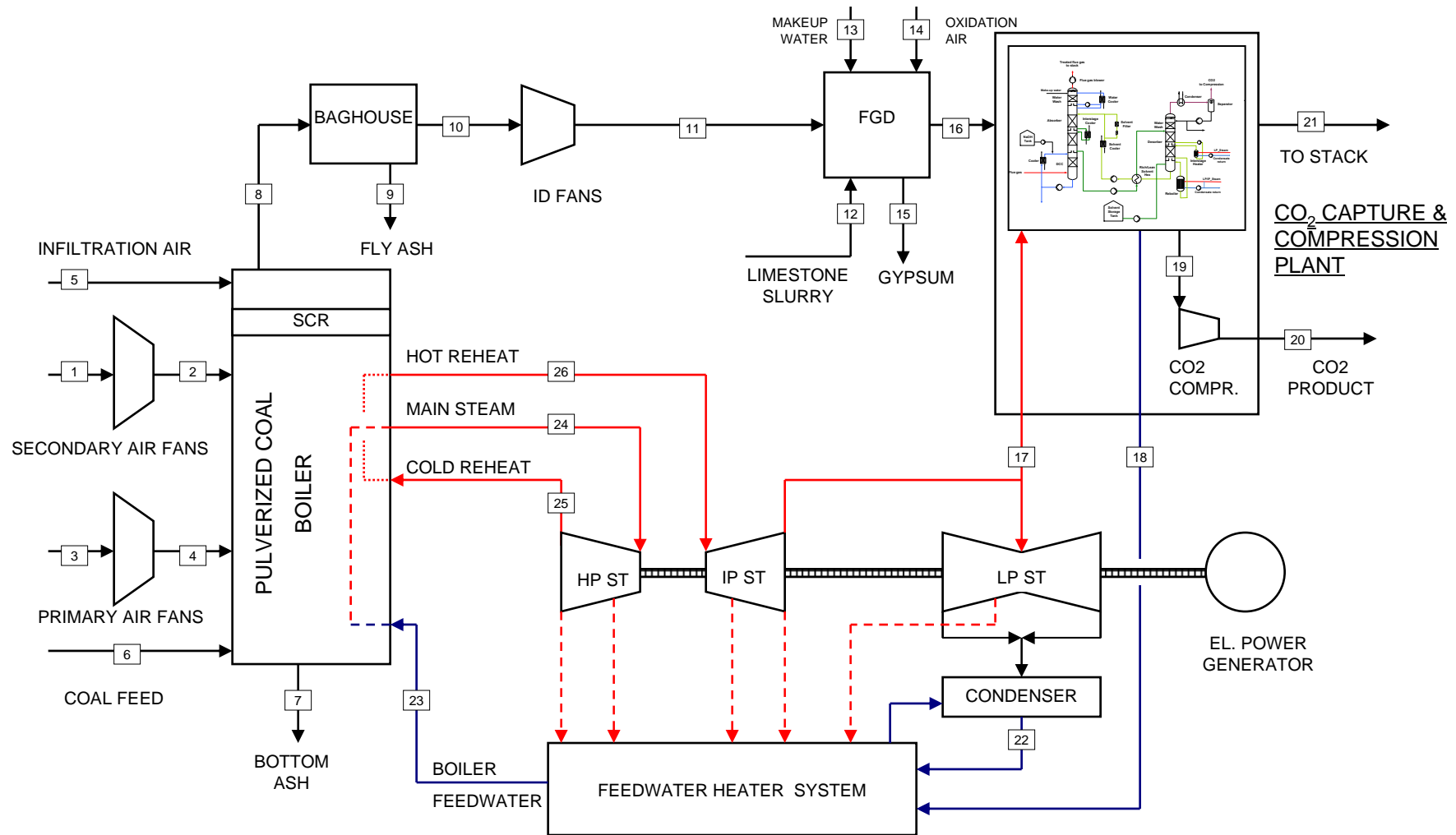
- Brian Research & Engineering ProMax[®] software for PCC parametric optimization
- BASF's proprietary package for rigorous solvent performance predictions



PCC – Power Plant Typical Process Integration Option (LB-1)



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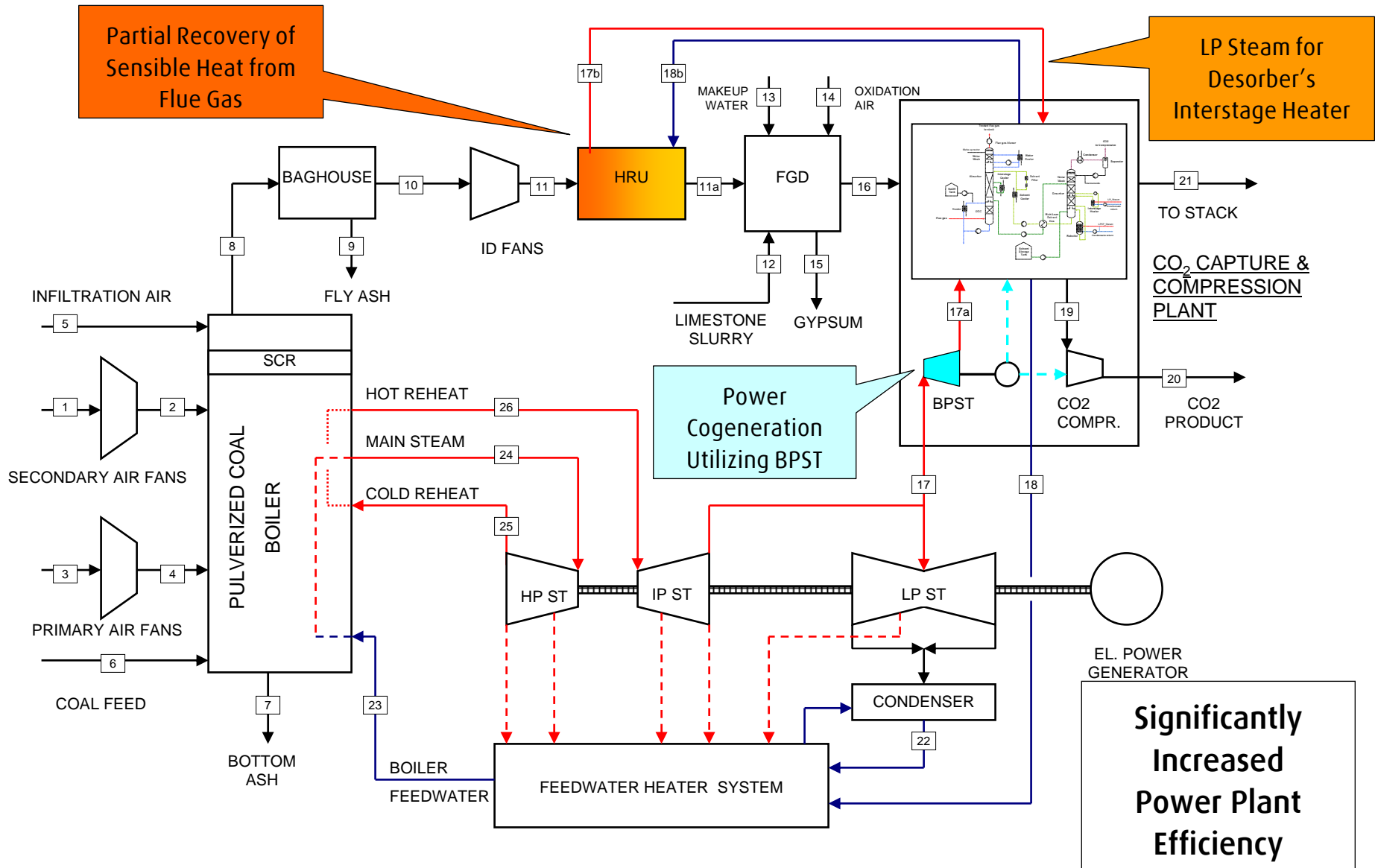


PCC – Power Plant Advanced Process Integration Option (LB-2)

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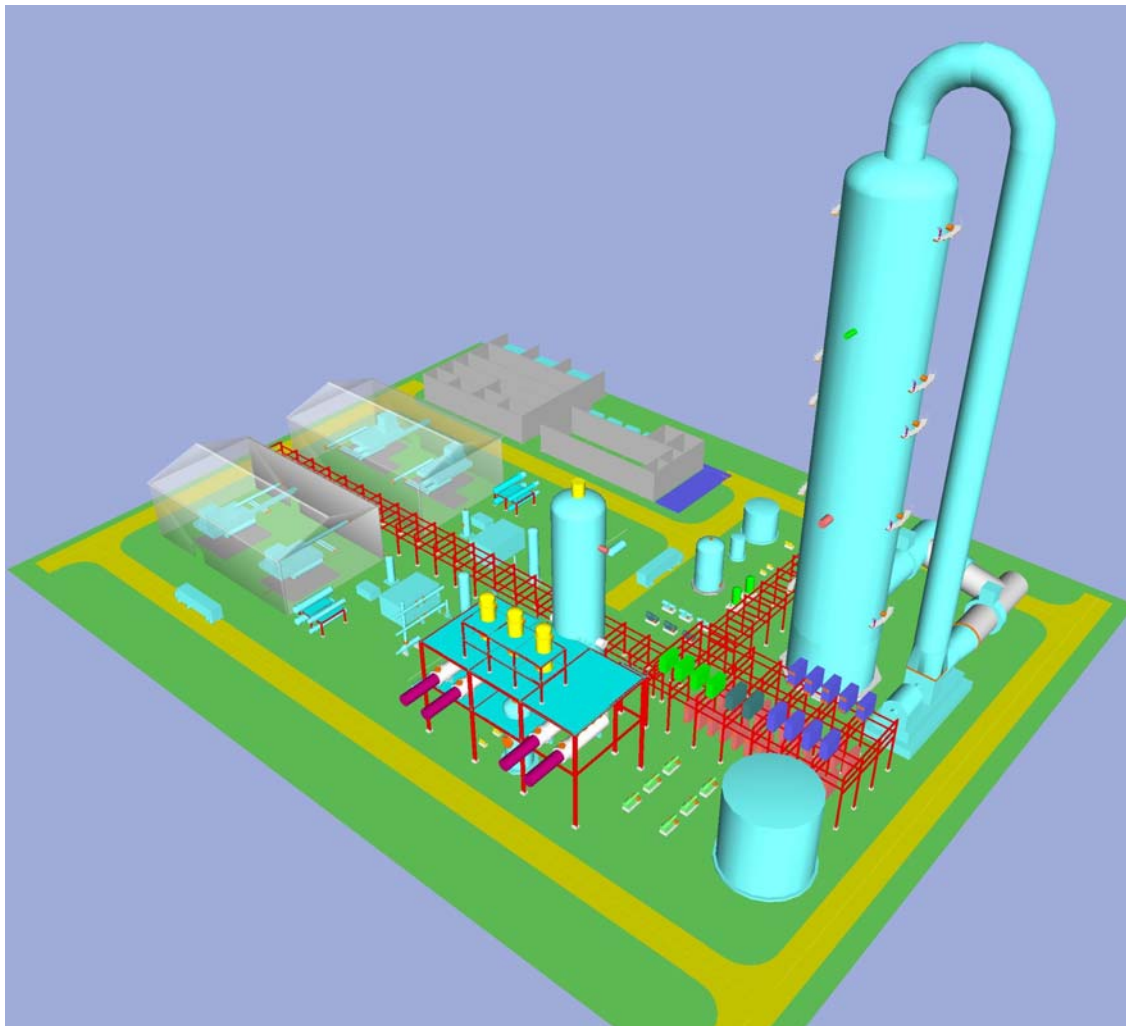


Linde-BASF PCC Plant Design for 550 MWe PC Power Plant

BASF
The Chemical Company

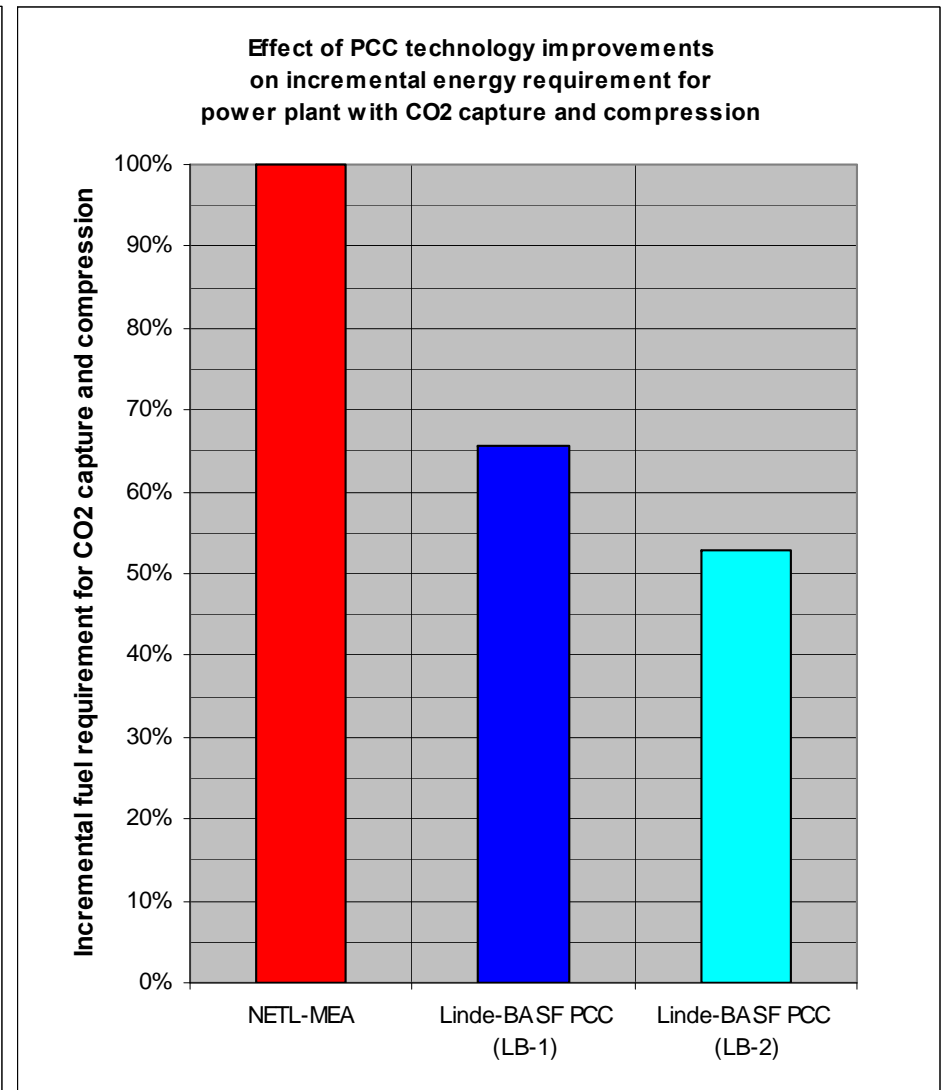
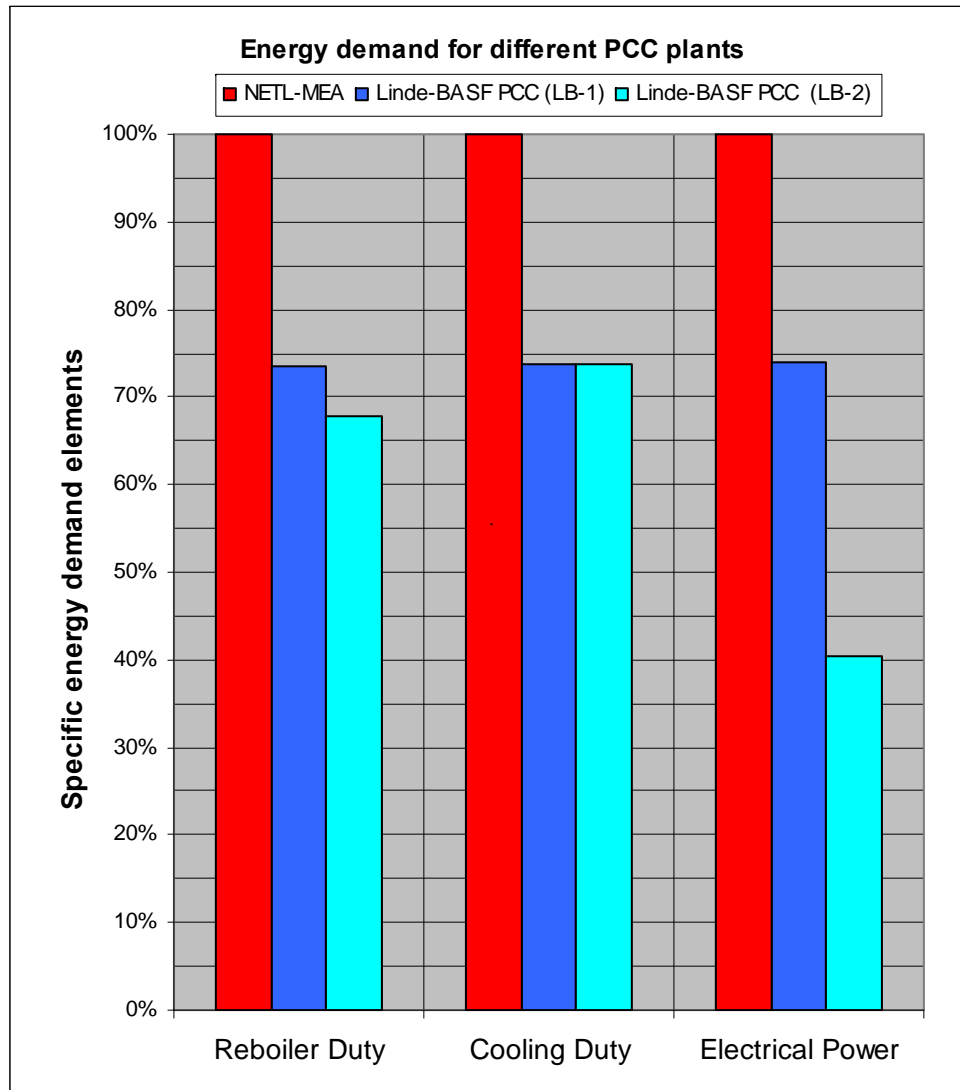
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- ❑ Single train PCC design for ~ 13,000 TPD CO₂ capture
- ❑ 40-50% reduced plot area to 180m x 120 m

Comparative PCC Performance Results Linde-BASF vs Reference DOE/NETL Case*

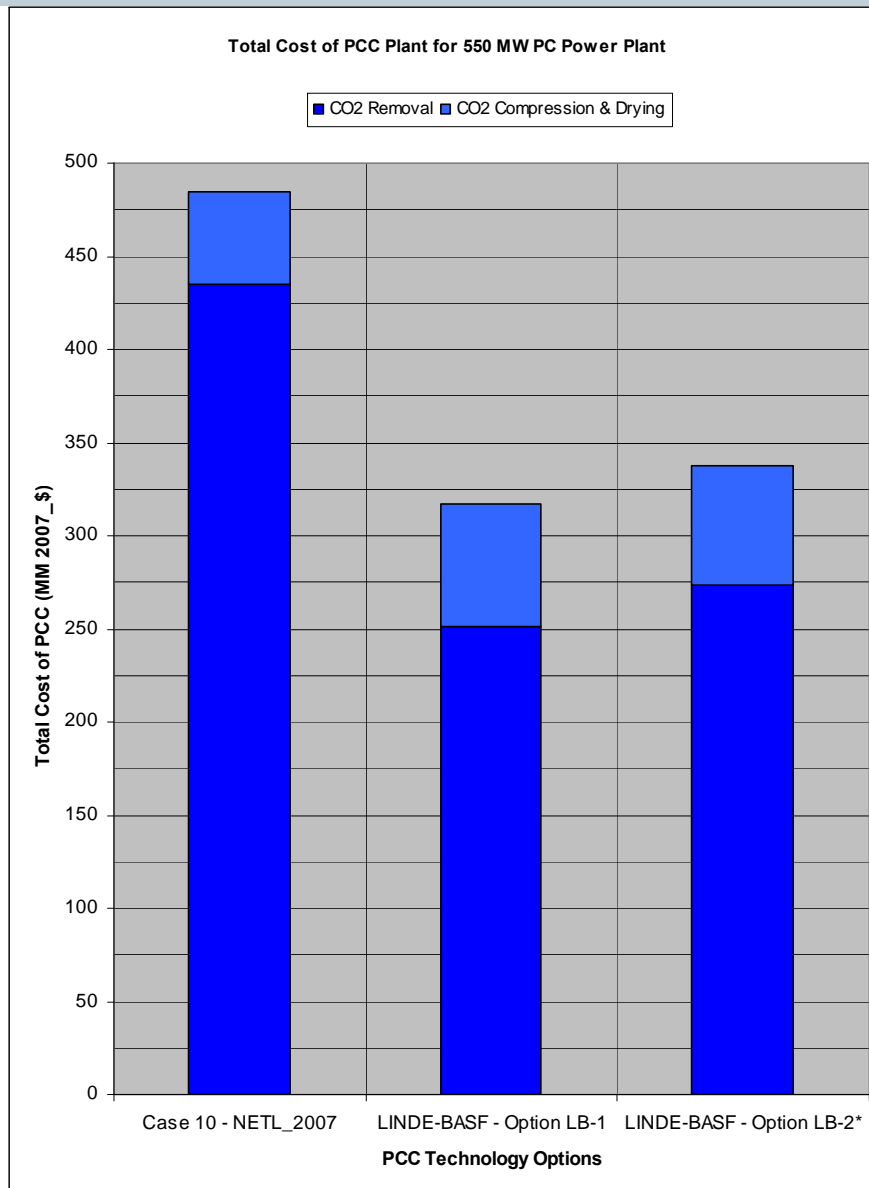


* Reference Case # 10 of DOE-NETL 2007/1281 Report

Total PCC Plant Cost



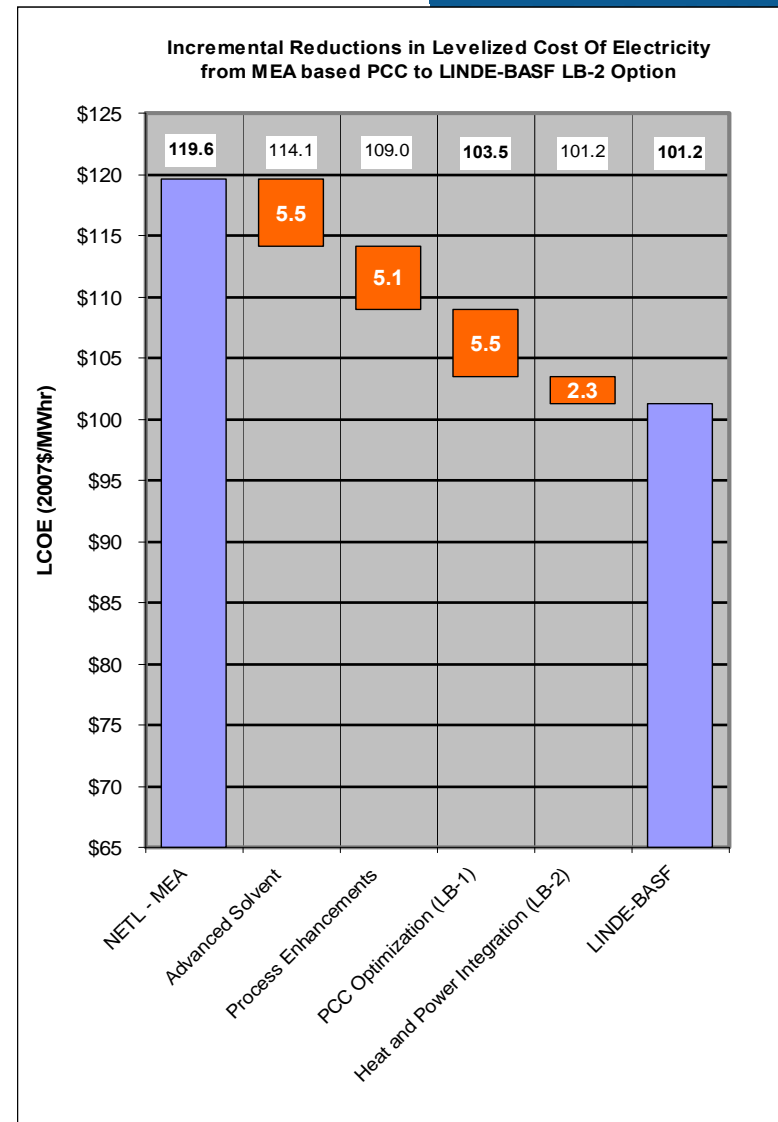
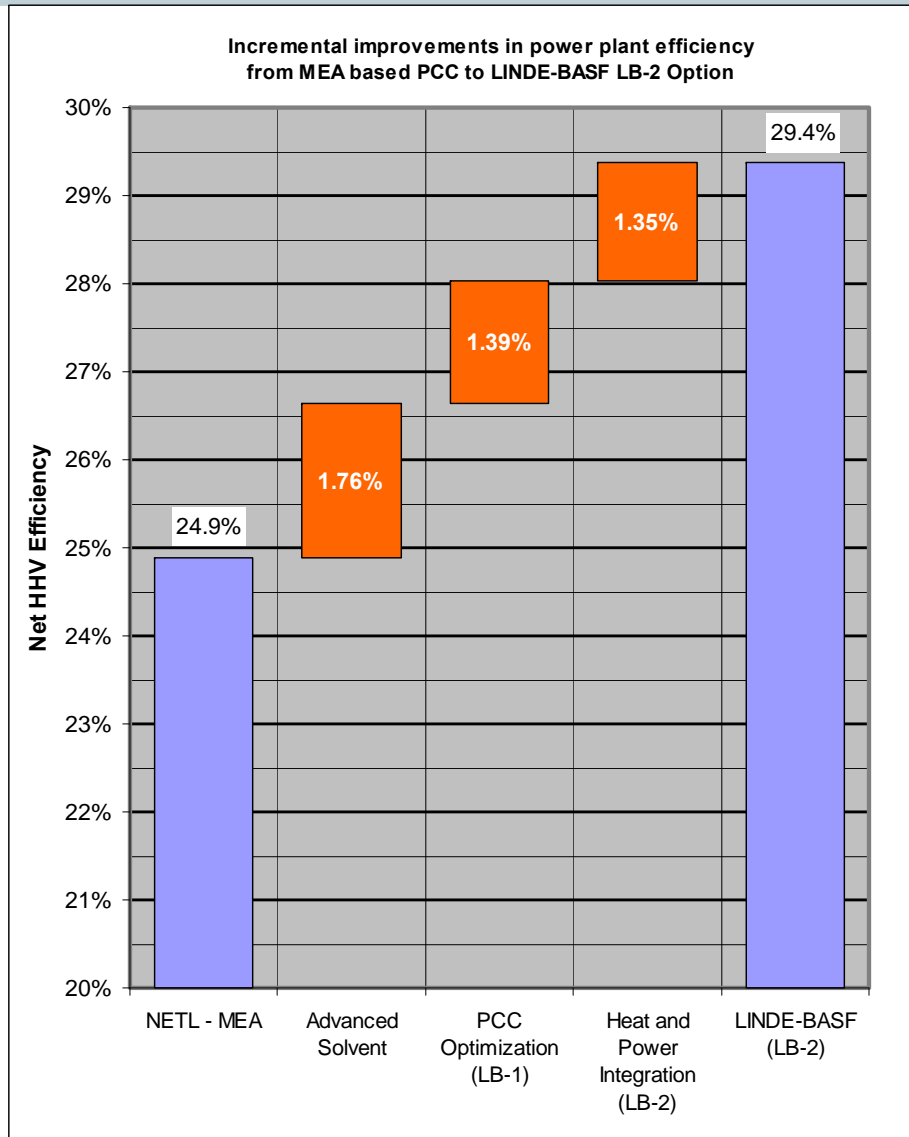
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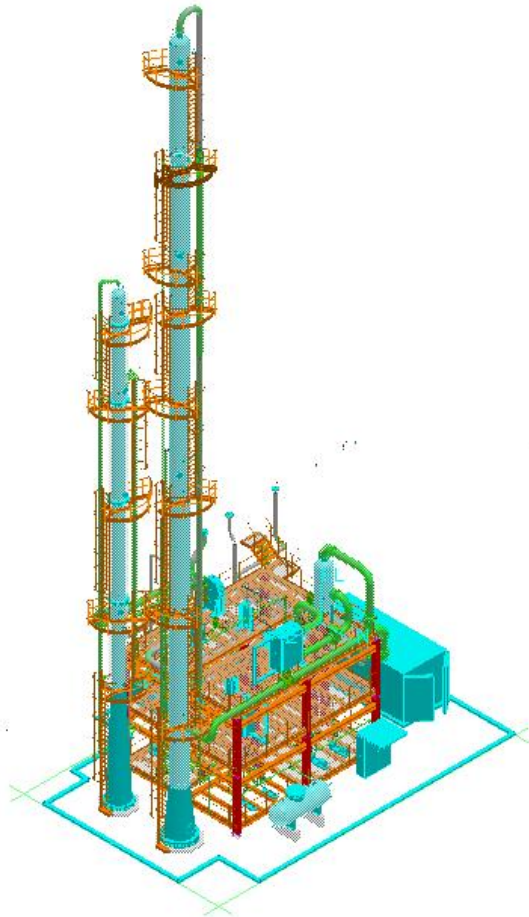
Significantly reduced total PCC plant Cost relative to DOE/NETL 2007 Reference Case #10 due to

1. Reduced coal combustion (CO2 production) for 11.1% (LB-1) or 15.2% (LB-2)
2. Single train PCC design
3. Optimized PCC plant design

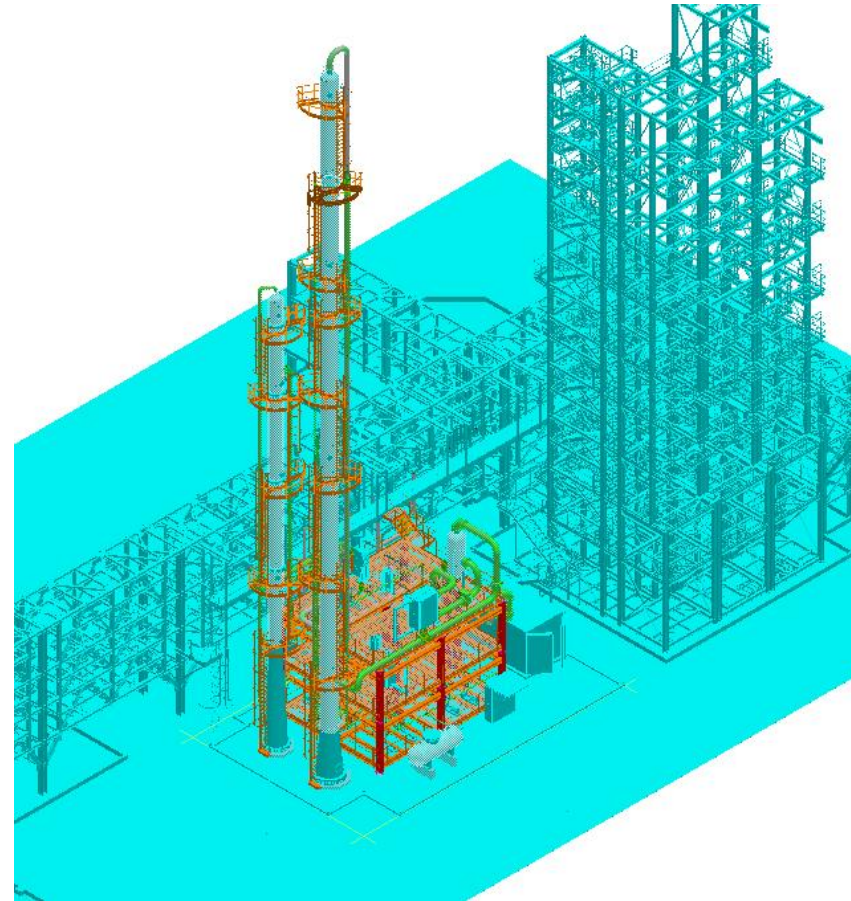
Power plant efficiency improvements and LCOE reductions with Linde-BASF PCC technology



Detailed Engineering Model of Pilot Plant



- Free-standing absorber and stripper
- Equipment modules containing pumps, blower, HX etc



Pilot plant located in NCCC site with the existing 0.5 MWe pilot and piperack in the background

Summary and Next Steps

- Linde and project partners are designing and building a 1 MWe post-combustion capture pilot plant to be installed and tested at the National Carbon Capture Center in Wilsonville, AL.
- The plant will incorporate BASF's OASE[®] blue solvent technology and Linde-BASF process enhancements and demonstrate that target performance can be achieved.
- Techno-economic assessment on a 550 MWe coal-fired power plant has confirmed the significant energy and capex savings compared to a reference MEA PCC plant, thereby, driving down the levelized cost of electricity.
- Critical next steps for the project:
 - Complete detailed engineering of the pilot plant and firm cost estimates and reach "Go" decision to proceed pilot plant procurement and build (Budget Period 1)
 - Procure, fabricate and install pilot plant at the NCCC and achieve mechanical completion (Budget Period 2)
 - Perform parametric and long duration tests and confirm achievement of target performance. (Budget Period 3)

Acknowledgement and Disclaimer

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Thank you for your attention!

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